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Practical role of racemization rates in deracemization kinetics and process productivities

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Supporting Information Placeholder

ABSTRACT: Herein, we report the chiral symmetry breaking of 2-methoxy-1-naphthamide atropisomers through temperature cycling without the use of any racemization reagent. The racemization rate (k_1) controls the deracemization process when the cooling of the slurry is slow enough to keep the system close to equilibrium. The productivity appears proportional to the racemization rate (k_1) multiplied by the solubility.

Chirality has attracted research interest for many years. Among many of its fascinating facets, chiral resolution, i.e., the process by which two mirror-image molecules are separated from their mixture, is of paramount importance in chemistry.^{1–3} In the context of the pharmaceutical industry, this has led to the stringent requirement that any new chiral pharmaceutical ingredient be developed in its active enantiopure form.^{4,5} Hence, resolution procedures are important; optimization facilitated by a fundamental understanding of the resolution process is key to the successful application of these techniques in industry.

Among the different chiral-resolution techniques available to the engineer,^{6–9} deracemization is an attractive process because its theoretical yield is 100%, whereas the yield from other methods cannot exceed 50%. Although many techniques, for example grinding,^{10,11} ultrasound,¹² homogenization,¹³ temperature cycling,^{14,15} and microwave¹⁶ have been applied to deracemization processes, temperature cycling is considered to be the most favourable technique from an industrial perspective because of its simplicity and applicability to a wide range of compounds. Also, in the context of the universal origin of chirality, temperature cycling is found in the natural day/night cycle, which might induce (or promote) deracemization in a natural system. Hence, clarification of the key parameter(s) that control(s) deracemization processes through temperature cycling is urgently required, not only from an industrial viewpoint, but also from the perspective of gaining a universal understanding of symmetry breaking.

While many molecules have been deracemized, several researchers have attempted to experimentally identify the key parameters that control these processes.^{17–30} The results of these studies suggest that racemization and crystal-growth/dissolution rates are essential factors that govern the efficiency of a deracemization procedure. This observation is in good agreement with that of Igglund and Mazzotti, who focused on computational simulations of the isothermal Viedma ripening process, and showed that the ratio of these rates is the key criterion that controls the deracemization

rate.²⁶ However, in the case of deracemization by temperature cycling, dissolution/growth rates are mainly controlled by the temperature profiles.

Consequently, when dissolution and crystal growth are performed smoothly, racemization rates should be, in principle, the key parameter in deracemization kinetics. In addition, if the racemization rate alone is a good proxy for estimating deracemization, it will provide a high level of practical convenience.

Despite this background, the quantitative role of racemization rate on deracemization kinetics has not been considered experimentally yet because of the difficulties associated with experimental systems. Indeed, most of the published deracemization studies focus on chiral compounds containing stereogenic centres that follow complicated deracemization kinetics because an additional component (e.g. a base) is added to the system, thereby adding an additional level of complexity to the problem.³¹ The deracemization of atropisomers elegantly circumvents this issue.¹¹ Indeed, atropisomerism arises from axial chirality and is due to restricted rotation about a single bond; accordingly, its racemization is a unimolecular process that should follow first-order reaction kinetics characterized by a single parameter.

In this context, we prepared naphthamide **1** as a compound that racemizes in a simple manner and forms in conglomerate system. Indeed, compound **1** exhibits frozen atropisomerism in its solid-state, whereas it spontaneously racemizes in solution. Naphthamide **1** has previously been reported by Sakamoto et al.,³² and our sample was synthesized using a similar route (Scheme 1), the details of which can be found in the Supporting Information. Large single crystals (5–30 mg) for racemization-rate experiments were also prepared by the slow evaporation of a saturated 1:1 (v/v) CHCl₃:heptane solution.

Scheme 1. Synthesis of the 2-methoxy-1-naphthamide **1**.

Sakamoto et al. reported the racemization rate constant (k_1) for **1** in methanol (MeOH), tetrahydrofuran (THF), and a 1:1 mixture of MeOH and THF.³² Here, we measured k_1 in various solvents including alcohols, ketones, nitriles, and ethers. A large single crystal (consisting of only one chiral form) was dissolved in a solvent and the time dependence of the optical rotation at 365 nm was recorded over a few hours using a polarimeter. Hence, the slope of $\ln[\alpha_t/\alpha_0]$

as a function of time was used to determine the first-order racemization rate constant k_1 . The racemization rate was evaluated in terms of racemization rate constant k_1 .

The solubilities and racemization rate constants (k_1) of **1** in the solvents considered are summarized in Table S1 in the Supporting Information. Generally, k_1 was higher in the less-polar solvents. For example, k_1 increased linearly with increasing solvent chain length in the nitrile solvents. Although the racemization rate constants were highest in the ether solvents, solubility was relatively low. The racemization rate constants were much lower in the alcohol series than in other types of solvent. These observations are ascribable to hydrogen bonding between the carbonyl oxygen of **1** and the solvent, which reduces the rate of racemization. Although Sakamoto et al. reported that **1** retains its chirality in MeOH through hydrogen-bonding interactions,³² our systematic study reveals that **1** racemizes at a rate depending on the solvent polarity; this trend is particularly conspicuous within the same solvent series.

Deracemization experiments involving **1** were carried out in *t*BuOH, MTBE, MIBK, and *i*PrCN by temperature cycling of the saturated solution in equilibrium with the crystals, as described in the following procedure. First, the atropisomer was dissolved in the solvent and the solution was filtered through a membrane filter. The filtered solution was maintained at 20 °C until crystallization spontaneously occurred. The first crystals are usually slightly (< 3%) randomly enriched with one enantiomer. Temperature cycling was then performed between 20 and 25 °C for 5–7 d. The enantiomeric excess of the solid was monitored by optical rotation every 24 h. Since the cooling from 25 to 20 °C corresponds to the crystal-growth step, it was conducted more slowly than the other steps in order to prevent an uncontrolled nucleation of the counter enantiomer. We showed in this study that the racemization of **1** occurs very slowly in cold methanol (MeOH); therefore, these conditions were selected to evaluate optical rotation and to mitigate the racemization of **1**.

It should be noted that 20% of the crystal mass was deliberately dissolved during heating in order to directly compare the deracemization rates in different solvents (Figure 1). The solution equilibria after the heating and cooling steps were confirmed in the same manner used in gravimetric-solubility experiments; i.e., the times for dissolution and crystal growth were sufficient as not to be the rate-limiting steps in the experiment.

Compound **1** was efficiently deracemized within a few days with final enantiomeric excesses (*ees*) greater than 90% in *t*BuOH,

Figure 1. Schematic illustration of the deracemization experiment.

MTBE, MIBK, and *i*PrCN, through temperature cycling, with or without an initial chiral bias (Figure 2). The crystal form obtained by deracemization was the same as that reported earlier.³²

The evolution of enantiomeric excess was sigmoidal in nature. This behaviour is often observed in solid-state deracemizations. The dominant enantiomer was determined by the initial chiral bias, except in the *i*PrCN system. Indeed, in the latter case, when the

Figure 2. Enantiomeric excess (*ee*) values of the collected crystals of **1** as functions of time during deracemization experiments, and the corresponding t_{90-10} values in (a) MIBK, (b) *t*BuOH, (c) MTBE, and (d) *i*PrCN. Each point includes uncertainty (< $\pm 1.5\%$) due to the polarimetry technique.

process was slightly (–)-enriched, deracemization occurred with the formation of the (opposite) (+)-isomer. Although we observed this phenomenon on two occasions, we are currently unable to provide an explanation for this observation.

To compare the deracemization rates under different conditions, Igglund and Mazzotti used the time required for the racemic mixture (0% *ee*) to reach 90% *ee* in order to evaluate isothermal Viedma ripening in their computational work.²⁶ Here, we define the time required to reach 90% *ee* from a slightly enriched state (10% *ee*), to be t_{90-10} , which excludes unreproducible behaviour often observed at the start of the deracemization process. For example, chirality in the solid state can deviate to one enantiomer and then heads in the opposite direction. The t_{90-10} values reported in Figure 2 are the averages of experiments conducted in triplicate.

According to Igglund and Mazzotti, deracemization kinetics is correlated theoretically to the ratio between the racemization rate and the crystal growth/dissolution rate.²⁶ However, as mentioned earlier, the cooling/heating steps were sufficiently slow, see also supporting information, to ensure that the suspension remains close to equilibrium; consequently these steps are not rate limiting and can be excluded when considering the overall deracemization rate in the experiment. Thus, herein, we considered the influence of the racemization rate on the global deracemization rate.

Figure 3a displays a plot of the natural logarithm of k_1 as a function of t_{90-10} using the experimental data collected herein for **1** in the four different solvents. It reveals that the deracemization rate can be estimated by simply measuring the racemization rate in the case of temperature cycling. Contextualising to real phenomena, these parameters can be intuitively interpreted as follows. Slow racemization in solution retains chirality for long periods of time and crystallization occurs with the same chirality before dissolution; therefore, deracemization proceeds at a sluggish pace. By contrast, the solution remains racemic during fast racemization, even during crystallization, which contributes to deracemization.

This behaviour qualitatively rationalizes other results obtained experimentally for deracemization; for example, Breveglieri et al. recently reported the deracemization of N-(2-methylbenzylidene)phenylglycine amide (NMPA) with DBU through temperature cycling, and concluded that a high operating temperature leads to fast deracemization.¹⁵ Racemization of NMPA with DBU can be

Figure 3. (a) Time required to achieve an *ee* of 90% (t_{90-10}) as a function of natural logarithm of the racemization rate (k_1). (b) The product of k_1 and solubility as a function of deracemization productivity.

considered to be a catalytic reaction; consequently, the racemization rate is higher at higher operating temperatures. The faster deracemization kinetics at higher temperature for NMPA with DBU is, according to our interpretation, mostly due to the high racemization rate of NMPA.

Moreover, we found that the deracemization productivity, which is defined by how much of the desired enantiomer is produced per unit time and volume of suspension, correlates linearly with the product of k_1 and solubility, as shown in Figure 3b. In terms of the global outcome of the process, k_1 controls the deracemization time, and solubility determines the scale of the symmetry breaking; hence, their product provides the productivity. For example, MTBE yields the fastest deracemization, but it is the worst medium in terms of productivity because of the poor solubility. This contrast illustrates that the order of the productivity differs from that of the deracemization rate. Thus, to achieve practically feasible applications of the process, it is very important to consider the balance between k_1 and the solubility.

In summary, we reported the first deracemization study of a single-component atropisomer through temperature cycling without the use of any racemization reagent. We also measured the racemization rates of the compound in different solvents to understand its influence on the overall deracemization rate. Our study suggests that the racemization rate (k_1) is the key parameter that determines the deracemization kinetics during temperature cycling. When considering once again the report of Breveglieri et al.,¹⁵ the faster deracemization kinetics at higher temperature for NMPA is probably also due to the higher solubility of NMPA.

Nevertheless, when the productivity of the global process is of interest, the product of racemization rate by solubility becomes the key parameter to consider. In this context, further process understanding can also be gained by studying the influence of impurities and cooling rate on the process kinetics, in addition to the starting particle-size distribution.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the ACS Publications website.

Synthesis of 2-methoxy-1-naphthamide, and (2-methoxynaphthalen-1-yl)(pyrrolidin-1-yl)methanone, racemisation kinetics, crystal growth rate, deracemisation experiments (PDF), Movies monitoring crystal growth in MIBK (AVI).

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Notes

The authors declare no competing financial interests.

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